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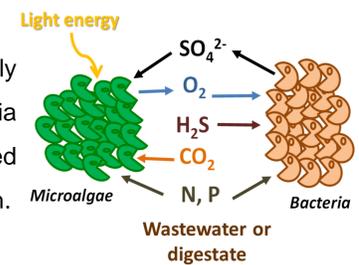
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INTRODUCTION

Based on its high CH₄ content (40-75%), **biogas** is considered a renewable energy source for the production of heat and power. **H₂S removal** is mandatory due to its toxicity and hazards associated with the corrosion of metals, while **CO₂ removal** increases the specific calorific value and reduces biogas costs of compression and transportation [1].

Biogas upgrading in algal-bacterial photobioreactors constitutes a cost-effective and environmentally friendly alternative for the removal of both contaminants [2]. These processes are based on the CO₂ consumption by microalgae via photosynthesis and the oxidation of H₂S to sulfate by sulfur-oxidizing bacteria using the oxygen photosynthetically produced [3]. In addition, domestic wastewater or anaerobic effluents can be used as nutrient source to support algal-bacterial growth.



MATERIALS AND METHODS

The experimental set-up consisted of a 9.6 m³ high rate algal pond (HRAP) interconnected to a 7 m³ settler and a 150 L bubble column.

Operating conditions:

HRAP recirculation velocity: 25 cm s⁻¹
HRT-HRAP: 3.5 days
HRT-settler: 7 hours

Domestic wastewater composition

NH ₄ ⁺ (mg L ⁻¹)	41.1±3.9
N-NO ₃ (mg L ⁻¹)	0
N-NO ₂ (mg L ⁻¹)	0
PO ₄ ³⁻ (mg L ⁻¹)	6.1±0.2
SO ₄ ²⁻ (mg L ⁻¹)	79.1±8.2
COD (mg L ⁻¹)	543.0±35.2
IC (mg L ⁻¹)	51.4±3.1

Raw biogas composition:

CH ₄ (%)	68.4±1.7
CO ₂ (%)	34.0±1.8
H ₂ S (ppm)	2069±991

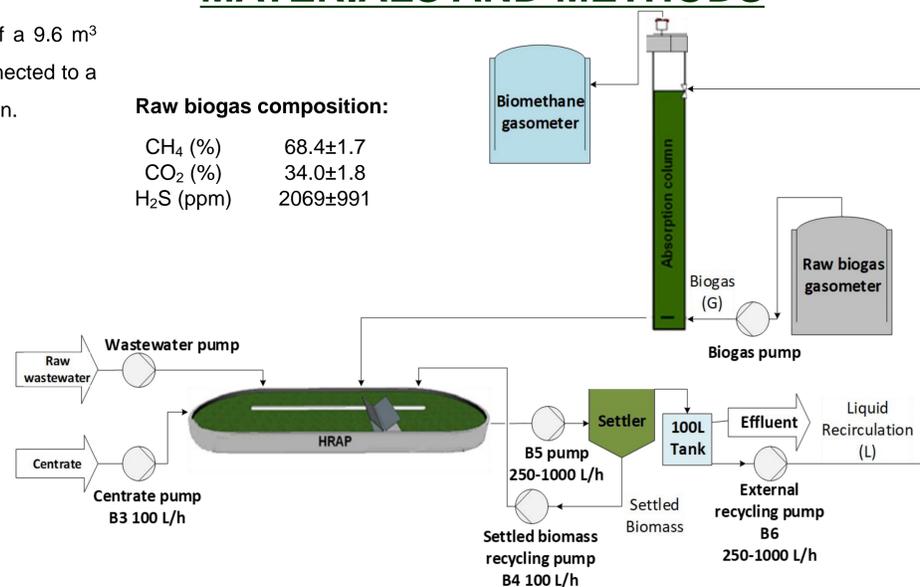


Figure 1. Schematic diagram (left) and photograph (right) of the continuous biogas upgrading experimental plant at Aqualia's facility in Chiclana

RESULTS AND DISCUSSION

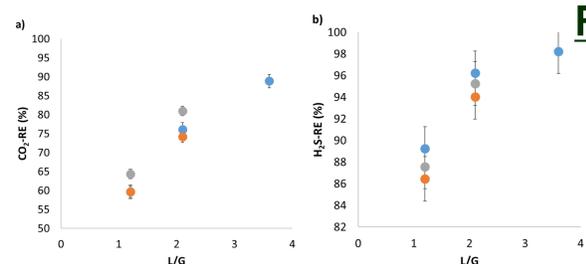


Figure 2. Influence of the L/G ratio on a) CO₂-RE, b) H₂S-RE at a biogas flowrate of 261 (●), 377 (●) and 471 L/h (●).

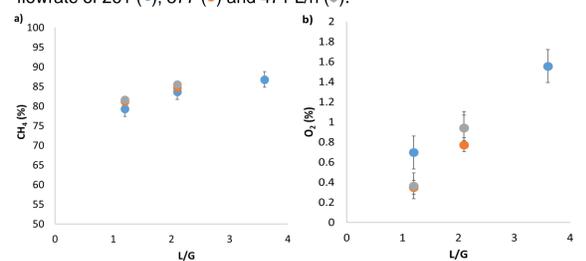


Figure 3. Influence of the L/G ratio on bio-methane composition: a) CH₄, b) O₂ at biogas flowrate of 261 (●), 377 (●) and 471 L/h (●).

Enhancements in CO₂ and H₂S removal efficiencies (REs) were observed with the increase in the liquid to biogas ratio (L/G).

The highest CH₄ concentration was 86.8±1.4 % at a L/G of 3.6 as a result of the high O₂ and N₂ content in the upgraded biogas.

A decrease in the pH of the recirculating cultivation broth from 7.95±0.08 to 6.69±0.30 was measured between the bottom and the top of the absorption column due to the acidic nature of CO₂ and H₂S.

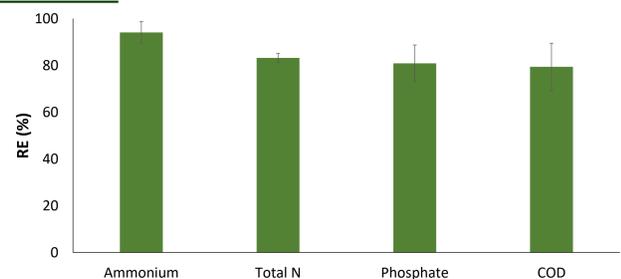


Figure 4. Ammonium, total nitrogen, phosphate and COD removal efficiencies in the system.

Table 1. Effluent composition

COD (mg L ⁻¹)	99.4±31.3
N-NH ₄ ⁺ (mg-N L ⁻¹)	1.9±1.5
N-NO ₂ (mg-N L ⁻¹)	0.2±0.1
N-NO ₃ (mg-N L ⁻¹)	1.9±1.0
PO ₄ ³⁻ (mg L ⁻¹)	1.2±0.4
SO ₄ ²⁻ (mg L ⁻¹)	136.5±13.5
IC (mg L ⁻¹)	25.6±5.5

COD: Chemical Oxygen Demand
IC: Inorganic Carbon

CONCLUSIONS

- ✓ The influence of L/G ratio on CO₂ and H₂S removal efficiencies was significant with the increase in CO₂-RE and H₂S-RE at higher L/G ratios. However, an increase in the L/G ratio promoted a higher desorption of O₂ and N₂ contained in the recycling liquid, which negatively impacted on the CH₄ concentration in the upgraded biogas.
- ✓ No significant effect of biogas flowrate on biomethane composition was observed.
- ✓ The effluent obtained complies with the EU Directive discharge requirements.
- ✓ An increase in the pH or alkalinity of the cultivation broth could enhance CO₂ and H₂S absorption at lower L/G.

REFERENCES

- ❖ [1] Toledo-Cervantes A., Serejo M., Blanco S., Pérez R., Lebrero R., Muñoz R., (2016). Photosynthetic biogas upgrading to bio-methane: Boosting nutrient recovery via biomass productivity control. *Algal Res.* 17, 46-52.
- ❖ [2] Bahr M., Díaz I., Domínguez A., González A. and Muñoz R. (2013). Microalgal-Biotechnology as a platform for an integral biogas upgrading and nutrient removal from anaerobic effluents. *Environ. Sci. Technol.* 2014, 48, 573-581.
- ❖ [3] Posadas E., Serejo M.L., Blanco S., Pérez R., García-Encina P.A. and Muñoz R. (2015). Minimization of biomethane oxygen concentration during biogas upgrading in algal-bacterial photobioreactors. *Algal Res.* 12: 221-229.

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